## We claim:

1. A process for the preparation of L-Threonine-O-(1,1-dimethylethyl)-1,1-dimethylethyl ester of formula (I)

## comprising:

A) contacting a compound having the formula

L-Threonine

B) with

Isobutylene

- C) in presence of mineral acid in an ether solvent for sufficient time; and
- D) purifying the L-Threonine-O-(1,1-dimethylethyl)-1,1-dimethylethyl ester.
- 2. A process according to claim 1, wherein molar ratio of L-Threonine and Isobutylene is between about 1:30 to 1: 50 more preferably between about 1:35 to 1: 45.
- 3. The process of claim 1, wherein the solvent is an ether solvent.
- 4. The process of claim 3, wherein the solvent is dimethoxyethane.
- 5. A process according to claim 1, wherein acid is mineral acid.
- 6. The process of claim 5, wherein mineral acid is sulfuric acid.

- 7. The process of claim 6, wherein sulfuric acid is concentrated.
- 8. The process of claim 7, wherein concentrated sulfuric acid is added between about -10 to 15 °C.
- 9. A process according to claim 1, wherein reaction mixture is stirred more than 10 hours.
- 10. The process of claim 9, wherein the temperature of the reaction mixture is between about -10 to 20 °C.
- 11. A process according to claim 10, wherein the reaction mixture after the formation of product of formula (I) is poured into a mixture of water and ammonia.
- 12. The process of claim 11, wherein water and ammonia mixture comprises between about 1:1 to 10:1.
- 13. The process of claim 12, wherein water and ammonia mixture is cold.
- 14. The process of claim 13, wherein temperature of the water and ammonia mixture is between about 0 to 15 °C.
- 15. A process according to claim 11, wherein an organic solvent is added to the crude product already poured into water and ammonia mixture.
- 16. The process of claim 15, wherein added organic solvent is an ether.
- 17. The process of claim 16, wherein ether is Dimethoxyethane.
- 18. The process of claim 17, wherein after extraction Dimethoxyetane layer is concentrated to get crude compound of Formula (I) in more than 90 % pure form.
- 19. The process of claim 18, wherein crude product is purified by vacuum distillation.
- 20. The process of claim 19, wherein pressure is reduced to 1 mm of Hg during distillation.
- 21. The process of claim 20, wherein pure fraction is collected between about 65 to 105 °C.
- 22. The process of claim 21, wherein pure fraction is collected more preferably between about 75 to 95 °C.
- 23. A process according to claim 1, wherein purity of formula (I) compound is about 99 %.